

Reg. No.



# Manipal Institute of Technology, Manipal

(A Constituent Institute of Manipal University)



## IV SEMESTER B.TECH (CHEMICAL ENGINEERING)

END SEMESTER EXAMINATIONS, June/July 2016

SUBJECT: MASS TRANSFER - I (CHE 203)

REVISED CREDIT SYSTEM

Time: 3 Hours

MAX. MARKS: 100

### Instructions to Candidates:

❖ Answer **FIVE FULL** questions. Missing data may be suitably assumed.

<b>1a</b>	Porous Alumina spheres, 10 mm diameter, 25 % voids, were thoroughly impregnated with an aqueous potassium chloride, KCl solution, concentration $0.25 \text{ g/cm}^3$ . When immersed in pure running water, the spheres lost 75% of their salt content in 6 hrs The diffusivity of KCl in water is $1.84 \times 10^{-9} \text{ m}^2/\text{s}$ . Estimate the time for removal of 85% of dissolved solute if the spheres had been impregnated with potassium chromate, $\text{K}_2\text{CrO}_4$ sol. at a con. $0.28 \text{ g/cm}^3$ , when immersed in a running water containing $0.02 \text{ g/cm}^3$ . The average diffusivity of $\text{K}_2\text{CrO}_4$ in water is $1.14 \times 10^{-9} \text{ m}^2/\text{s}$ .	<b>15</b>
<b>1b</b>	Give the equations for Diffusion in porous solids (three cases)	<b>5</b>
<b>2</b>	Derive the flux equation for the following cases starting from the this $N_A = N x_A + J_A$ for gases and liquids : A) Steady state diffusion of A through non diffusing B B) Steady state diffusion of Equimolal counter current (assume fluids are in laminar or rest in both cases)	<b>20</b>
<b>3a</b>	Estimate mass transfer coefficient of air flowing with a velocity of 5 m/s through cylindrical tube which is made up of Naphthalene. The diameter of pipe is 25 mm (I.D.). $D_{AB} = 2.5 \times 10^{-6} \text{ m}^2/\text{s}$ , density of air is $1.2 \text{ kg/m}^3$ and viscosity is $1.8 \times 10^{-5} \text{ Pa.s}$ (Use three methods)	<b>8</b>
<b>3b</b>	Prove that the $k \propto D^n$ (mass transfer coefficient is proportional to diffusivity) where n ranges between 0.5 to 1 using <b>four theories</b> .	<b>12</b>
<b>4a</b>	Calculate the minimum liquid rate for given absorber and compute the number of stages with 1.5 times of minimum liquid rate. (counter-current) with following data. The gas in $0.5 \text{ m}^3/\text{s}$ at $26^\circ\text{C}$ and pressure of $1.09 \times 10^5 \text{ N/m}^2$ containing 3% by volume of benzene oil vapors. The removal of benzene is 95% is expected with wash oil which is entering the absorber with 0.005 mole fraction benzene. The relation of liquid and gas mole ratios as follows $Y/(1+Y) = 0.125 * X/(1+X)$	<b>15</b>
<b>4b</b>	Explain the properties of solvent gas absorption	<b>5</b>
<b>5a</b>	Explain the preparation and use of following adsorbents: Fullers earths, Activated clays, Bauxites, Alumina, Bone char Silica gel, Gas adsorbent carbon and synthetic polymer adsorbents	<b>10</b>
<b>5b</b>	What are the major parameters considered for choosing tray and packed towers.	<b>10</b>

<b>6a</b>	Explain and show the hysteresis of adsorption isotherm	<b>4</b>
<b>6b</b>	Define tray efficiency and local efficiency	<b>4</b>
<b>6c</b>	Prove that $E_{ME} = \frac{E_{MR}}{E_{MR}(1-S) + S}$ where m is the slope of the equilibrium curve	<b>12</b>