



Manipal Institute of Technology, Manipal

(A Constituent Institute of Manipal University)



V SEMESTER B.TECH (CHEMICAL ENGINEERING)

END SEMESTER EXAMINATIONS, NOV/DEC 2015

SUBJECT: PROCESS DESIGN OF CHEMICAL EQUIPMENTS [CHE 301]

REVISED CREDIT SYSTEM

Time: 3 Hours

MAX. MARKS: 100

Instructions to Candidates:

- ❖ Answer **ANY ONE FULL** question.
- ❖ Missing data may be suitable assumed.

1A.	Explain in detail as to how the Economic pipe diameter is calculated using Genereaux method?	15																								
1B.	Estimate the size of hydrocyclone needed to separate 86% of particles with a diameter greater than 0.08 mm, from a dilute slurry with a flow rate of 1250 m ³ /day. The density of liquid is 1080 kg/m ³ and that of the solid is 3000 kg/m ³ , viscosity 1.5 mNs/m ²	15																								
1C.	<p>Synthesis gas has to be cooled from 250 °C to 25 °C. Cold water is available at 20 °C and the output is preferred at 40 °C. Design a suitable STHE for the process.</p> <p>DATA:</p> <table><tr><td></td><td>Gas mixture</td></tr><tr><td>Specific heat (KJ/kg K)</td><td>2.008</td></tr><tr><td>Density (kg/m3)</td><td>0.51</td></tr><tr><td>Viscosity (cP)</td><td>0.014</td></tr><tr><td>Thermal Conductivity (W/m K)</td><td>0.149</td></tr></table> <p>Composition of Synthesis gas is as follows: H₂ – 0.94665 ks/s, CO₂ – 11.066 ks/s, CO – 0.33 kg/s, CH₄ – 0.05 kg/s, N₂ – 0.081 kg/s ❖ Use Q_h = Q_c without any extra allowance</p>		Gas mixture	Specific heat (KJ/kg K)	2.008	Density (kg/m3)	0.51	Viscosity (cP)	0.014	Thermal Conductivity (W/m K)	0.149	70														
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2A.	<p>Carbon dioxide is to be absorbed from air at 24 °C and 1 atmosphere pressure using a 30% MEA solution entering with 0.06 moles of CO₂ on solute free basis. The entering gas has 6% O₂, 79% N₂ and the rest CO₂. It leaves with 2% CO₂. Design a counter current Sieve plate absorber. Data of X and Y are in solute free basis.</p> <table><tr><td>X</td><td>0.05</td><td>0.06</td><td>0.062</td><td>0.064</td><td>0.066</td><td>0.068</td><td>0.072</td></tr><tr><td>Y</td><td>6.0*10⁻³</td><td>14.23*10⁻³</td><td>32.8*10⁻³</td><td>65.4*10⁻³</td><td>0.1213</td><td>0.2047</td><td>0.3411</td></tr></table> <p>PROPERTIES</p> <table><tr><td>MEA mol. Wt. = 61.07 kg/kgmole</td><td>Liquid density = 1000 kg/m³</td></tr><tr><td>Gas viscosity = 0.0175 cP</td><td>Liquid viscosity = 1 cP</td></tr><tr><td>Gas diffusivity D_g = 0.163*10⁻⁴ m²/s</td><td>Liquid diffusivity D_l = 1.9*10⁻⁵ cm²/s</td></tr><tr><td colspan="2">σ of solution and water = 67.6 and 72.8 dyne/cm respectively</td></tr></table> <p>Important INFORMATION to be incorporated:</p> <ul style="list-style-type: none">• (L_m'/ G_m')_{op} = 1.25(L_m'/ G_m')_{min}• Use Φ_{dc} as 0.5	X	0.05	0.06	0.062	0.064	0.066	0.068	0.072	Y	6.0*10 ⁻³	14.23*10 ⁻³	32.8*10 ⁻³	65.4*10 ⁻³	0.1213	0.2047	0.3411	MEA mol. Wt. = 61.07 kg/kgmole	Liquid density = 1000 kg/m ³	Gas viscosity = 0.0175 cP	Liquid viscosity = 1 cP	Gas diffusivity D _g = 0.163*10 ⁻⁴ m ² /s	Liquid diffusivity D _l = 1.9*10 ⁻⁵ cm ² /s	σ of solution and water = 67.6 and 72.8 dyne/cm respectively		100
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