



MANIPAL INSTITUTE OF TECHNOLOGY
(A constituent institute of Manipal University)



VII SEMESTER. B.Tech. (MECHANICAL ENGINEERING)
END SEMESTER EXAMINATIONS, NOV/DEC 2015

SUBJECT: COMPUTATIONAL FLUID DYNAMICS (MME 441)
(REVISED CREDIT SYSTEM)

Time: 3 Hours.

MAX.MARKS: 50

Instructions to Candidates:

- ❖ Answer **ANY FIVE** full questions.
- ❖ Missing data may be suitably assumed.

- 1A** For the x-directional Navier-Stokes (Momentum) Equation (no derivation) use scaling laws to deduce **scale-free equation** as given below: **-04-**

$$\frac{\partial u'}{\partial t'} + u' \frac{\partial u'}{\partial x'} + v' \frac{\partial u'}{\partial y'} + w' \frac{\partial u'}{\partial z'} = -\frac{1}{F^2} - P \frac{\partial p'}{\partial x'} + \frac{1}{R} \left(\frac{\partial^2 u'}{\partial x'^2} + \frac{\partial^2 u'}{\partial y'^2} + \frac{\partial^2 u'}{\partial z'^2} \right)$$

where, prime sign indicate the corresponding scale-free properties and F and R represents the Dimensionless Froude and Reynold's Numbers where as $P = \frac{P_\infty}{\rho U_\infty}$ is the Non-dimensional Pressure Coefficient, with P_∞ and U_∞ being the free stream pressure and velocity where as ρ is the density of the medium.

- 1B** Derive the **Pressure Correction Equation** for Convection dominated Diffusion flow. Explain with a neat flow diagram SIMPLE algorithm of Patankar & Spalding **-06 -**

- 2A** Derive the continuity equation in the conservative form given by **-03-**

$$\frac{\partial}{\partial t} \iiint_V \rho dV + \iint_S \rho \mathbf{V} \cdot d\mathbf{S} = 0$$

- 2B** Water is flowing in a pipe of diameter 25 mm. It enters the pipe with a temperature of 150°C. The velocity at inlet is 8 m/s which can be assumed to remain constant along the pipe length. The diffusive flux (Γ) through the pipe can also be assumed to be constant at 800 kg/m/s. The length of the pipe is 900 mm. Water leaves the pipe at a temperature of 30°C. Apply the following discretization schemes and obtain the temperature distribution along the pipe **using Control Volume technique**. Use three equally spaced unknown control volumes to discretize the domain in each case. **-07-**
- (1) Central Difference Scheme (CDS)
 - (2) Upwind Differencing Scheme (UDS)
 - (3) Exact Analytical Method.

- 3A** Derive the non-dimensional form of the steady one dimensional convection-diffusion fluid flow equation and obtain the general solution in the standard form, **-06-**

$$\theta = \frac{\left(e^{PX} - 1 \right)}{\left(e^P - 1 \right)} \quad \text{where } P \text{ is the Peclet Number}$$

- 3B** Illustrate with a physical example Dirichlet, Neumann Cauchy and Robin Boundary conditions. **-04-**

- 4A** Explain the **Basic Four Rules** enunciated for control volume formulation. **-04-**

- 4B** What is meant by Numerical False Diffusion? Explain the same comparing the diffusive flux for UDS and CDS schemes. **-03-**

- 4C** Explain with neat grid arrangements the implementation of boundary conditions for: **-03-**

- (1) Inlet Conditions
- (2) Axisymmetric Condition
- (3) Exit conditions

- 5A** A steel fin of thermal conductivity 45 W/m.K and having uniform rectangular cross section 25mm X 20 mm and length 200 mm, is fitted to an engine head at 375°C. It is exposed to ambient convective air having convective heat transfer coefficient of 20 W/m².K. The average bulk temperature of the cooling air is 35°C. The fin can be treated as slender with negligible heat transfer from the open end face of the fin. Use **Finite Difference approach using Taylor series** to solve temperature distribution in atleast FIVE unknown grids assuming steady one dimensional heat transfer, using TDMA **-07-**

- 5B** What are the difficulties in solving the convection dominated diffusion problem? What are the strategies to be adopted to overcome them? **-03-**

- 6A** Compute the steady state temperature distribution along a one dimensional slender fin rod having 25 mm diameter and thermal conductivity of 50 w/m.K as shown in **Fig. 1** below. Set up the solution using Control Volume formulation. The fin is exposed to an ambient at 60 °C and a convective heat transfer coefficient of 15 W/m².K. Use TDMA for computation of grid temperatures. **-06-**

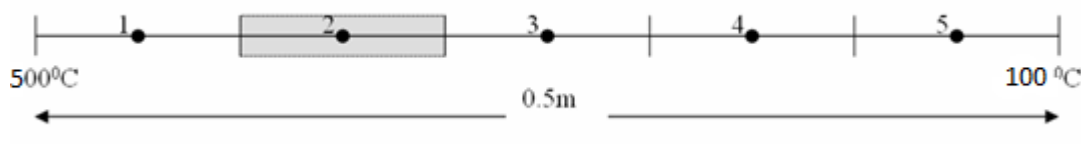


Fig. 1

- 6B** Explain with regard to finite difference discretization schemes the following: **-04-**
- (a) Consistency
 - (b) Boundedness
 - (c) Transportiveness
 - (d) Accuracy