| Reg. No. |  |  |  |  |  |  |  |  |  |  |
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Manipal Institute of Technology, Manipal

(A Constituent Institute of Manipal University)

## IV SEMESTER B.TECH (CHEMICAL ENGINEERING)

## END SEMESTER MAKEUP EXAMINATIONS, JUN/JUL 2017

SUBJECT: CHEMICAL ENGINEERING THERMODYNAMICS-II [CHE 2201]

## **REVISED CREDIT SYSTEM**

Time: 3 Hours

MAX. MARKS: 100

**Instructions to Candidates:** 

✤ Answer ALL questions.

✤ Missing data, if any, may be suitably assumed.

| 1Δ          | Determine the fugacity of a component at 150°C and 100 bar from the given data.                                      |                            |                           |              |             |              |                |              | 11 |
|-------------|--|----------------------------|---------------------------|--------------|-------------|--------------|----------------|--------------|----|
|             | P, bar   | 10                         | 20                        | 40           | 60          | 80           | 100            |              |    |
|             | Ζ  | 0.985                      | 0.970                     | 0.942        | 0.913       | 0.885        | 0.869          |              |    |
|             |  |                            |                           |              |             |              |                |              |    |
| 1B.         | The molar enthalpy of a component in a binary solution is given by the relation                                      |                            |                           |              |             |              |                |              | 09 |
|             | $H = (0.01x_1x_2)(3x_1 + 5x_2)$  |                            |                           |              |             |              |                |              |    |
|             | Where H is in J/mol. Determine $\overline{H_1}$ as function of $x_2$ and the numerical values of the                 |                            |                           |              |             |              |                |              |    |
|             | pure component enthalpy $H_1$ .  |                            |                           |              |             |              |                |              |    |
| 2A.         | Check whe  | ther the for $\frac{1}{2}$ | ollowing e                | quations sa  | tisfy Gibbs | s- Duhem e   | equations.     |              | 10 |
|             | $ln\gamma_1 = Ax_2^2$  | $5 + B\chi_2^2$            | $5x_1 - x_2$              |              |             |              |                |              |    |
|             | $m\gamma_2 - A\lambda_1$   | $[ \pm Dx_1 ($             | $x_1 - 3x_2$              |              |             |              |                |              |    |
| 20          | For a mixtu  | ure of ace                 | tic acid a                | nd toluene   | containing  | , 0.486 mo   | le fraction    | toluene, the | 06 |
| <b>ZD</b> . | partial pres   | sures of a                 | acetic acid               | and tolue    | ne are four | nd to be 0.  | 118 bar and    | d 0.174 bar  | 00 |
|             | respectively   | y at 343 H                 | K. The vap                | pour pressu  | ires of pur | e compone    | ents at this t | temperature  |    |
|             | are 0.269 t  | par and 0                  | .181 bar 1<br>aid is 0.55 | tor toluene  | and aceti   | c acid resp  | ectively. T    | he Henry's   |    |
|             | constant for acetic acid is 0.55 bar. Calculate the activity and activity coefficient for acetic acid in the mixture |                            |                           |              |             |              |                |              |    |
|             | (i) Based on Lewis –Randall rule.  |                            |                           |              |             |              |                |              |    |
|             | (ii)   | Based on                   | Henry's la                | aw.          |             |              |                |              |    |
|             |  |                            |                           |              |             |              | <u>a</u>       |              |    |
| 2C.         | Derive the   | expression                 | n for the e               | ffect of pre | ssure on ac | ctivity coef | ficient.       |              | 04 |
| 2 4         | Discuss the  | step by s                  | step procee               | dure for the | e construct | ion of P-x-  | y diagram,     | for an ideal | na |
| 3A.         | solution hav   | ving two o                 | componen                  | ts.          |             |              |                |              | 03 |
|             |  |                            |                           |              |             |              |                |              |    |
| 3B.         | Explain pos  | sitive and                 | negative d                | leviation fr | om ideality | y with the h | elp of P-x-    | y diagram.   | 06 |
|             |  |                            |                           |              |             |              |                |              |    |

| 3C. | The vapour pressures of acetone (1)- acetonitrile (2) is given by Antoine equations.<br>$lnP_1^s = 14.5463 - \frac{2940.46}{T-35.93}$<br>$lnP_2^s = 14.2724 - \frac{2945.47}{T-49.15}$<br>where T is in K and P is in kPa. Assuming the solutions formed are ideal. Calculate T and $y_1$ at 65 kPa and $x_1$ =0.4  |                             |                       |                               |                               |                            |                      |    |
|-----|---|-----------------------------|-----------------------|-------------------------------|-------------------------------|----------------------------|----------------------|----|
| 4A. | Verify whet $x_1$<br>$\gamma_1$   | her the follo<br>0<br>0.576 | 0.2<br>0.655<br>0.985 | are consisten<br>0.4<br>0.748 | t by zero are<br>0.6<br>0.856 | ea method.<br>0.8<br>0.950 | 1.0<br>1.00<br>0.379 | 10 |
| 4B. | <ul> <li>From VLE measurements for ethanol-benzene system at 318 K and 40.25 kPa, it is found that the vapour in equilibrium with a liquid containing 38.4% (mol) benzene contained 56.6% (mol) benzene. The system forms an azeotrope at 318 K. At this temperature the vapour pressures of ethanol and benzene are 22.9 and 29.6 kPa respectively. Determine the composition and total pressure of the azeotrope. Assume that van Laar equation is applicable for the system.</li> </ul>  |                             |                       |                               |                               |                            |                      |    |
| 5A. | A gas mixture containing 25% CO, 55% H <sub>2</sub> and 20% inert gas is to be used for<br>methanol synthesis. The gases are passed to a catalyst chamber where the following<br>reaction takes place<br>$CO(g) + 2H_2(g) \rightarrow CH_3OH(g)$<br>at a pressure of 300 bar and temperature of 625 K. Assume that the equilibrium<br>mixture forms an ideal solution and $k_f$ and $k_{\phi}$ are $4.9 \times 10^{-5}$ and 0.35 respectively.<br>What are the composition of all the components?   |                             |                       |                               |                               |                            |                      |    |
| 5B. | For the vapour phase hydration of ethylene to ethanol according to the reaction<br>$C_2H_4 + H_2O \rightarrow C_2H_5OH$<br>the standard heat of reaction at 298 K is $-45.95 \times 10^3$ J and the equilibrium constant<br>at 298 K is 14.86 The specific heat data is as follows.<br>$\hline C_p, J/\text{mol K}$ Ethylene $11.886 + 120.12 \times 10^{-3}T - 36.649 \times 10^{-6}T^2$<br>Water $30.475 + 9.652 \times 10^{-3}T + 1.189 \times 10^{-6}T^2$<br>Ethanol $29.358 + 166.9 \times 10^{-3}T - 50.09 \times 10^{-6}T^2$<br>Calculate the values of integration constants. |                             |                       |                               |                               |                            |                      | 08 |
| 5C. | List out the assumptions used for the establishment of vapour-liquid equilibrium in ideal solutions.  |                             |                       |                               |                               |                            |                      | 02 |