



## VI SEMESTER B.TECH (MECHANICAL ENGINEERING)

### END SEMESTER EXAMINATION – JUNE 2017

#### SUBJECT: HEAT TRANSFER (MME 3201)

#### REVISED CREDIT SYSTEM

**Time: 3 Hour**

**Max. Marks: 50**

**Note:** (i) Answer all questions

(ii) Missing data, if any, may be appropriately assumed

(iii) Draw the sketch as applicable

(iv) Assumptions made must be clearly mentioned

- 1A Derive an expression for steady state heat transfer through a composite wall. 04
- 1B Calculate the admissible current intensity for a 2 mm diameter copper wire covered with plastic insulation of optimum thickness so as to have positive heat transfer on the condition that the maximum temperature of insulation should not exceed  $60^{\circ}\text{C}$  and the temperature of the surrounding to be  $30^{\circ}\text{C}$ . The thermal conductivity of plastic is  $0.015\text{ W/m}^{\circ}\text{C}$  and the electrical resistance of the copper wire is  $0.005\ \Omega/\text{m}$ . Assume the surface heat transfer coefficient to be  $10\text{ W/m}^2\text{C}$ . 04
- 1C Explain the significance of Biot number in lumped system analysis. 02
- 2A Derive an expression for temperature distribution in a solid sphere in which one-dimensional radial conduction is taking place under steady state condition with uniform heat generation. 05
- 2B A steel tube carries steam at a temperature of  $330^{\circ}\text{C}$ . A thermometer pocket of iron ( $k = 48\text{ W/m}^{\circ}\text{C}$ ) of inside diameter  $16\text{ mm}$  and  $0.8\text{ mm}$  thick is used to measure the temperature. The error to be tolerated is 2 % of maximum. Estimate the length of the pocket necessary to measure the temperature within this error. The diameter of steel tube is  $80\text{ mm}$ . Assume  $h = 508\text{ W/m}^2\text{C}$  and tube wall temperature is  $120^{\circ}\text{C}$ . Suggest a suitable method of locating the thermometer pocket. 05
- 3A Using Buckingham's  $\pi$  theorem, derive all the non-dimensional variables for a forced convection system. 04
- 3B Lubricating oil of sp. gravity  $0.853$  flows at a rate of  $120\text{ kg/hr}$  through a  $10\text{ mm}$  diameter tube maintained at  $30^{\circ}\text{C}$ . Estimate the length of the tube required if the oil enters at  $80^{\circ}\text{C}$  and leaves at  $76^{\circ}\text{C}$ . Take property of oil at mean temperature as follows: 04
- $k = 0.13863\text{ W/m}^{\circ}\text{C}$ ,  $\nu = 41.6 \times 10^{-6}\text{ m}^2/\text{s}$ ,  $\text{Pr} = 546$ ,  $C_p = 2.139\text{ kJ/kg}^{\circ}\text{C}$
- $Nu = 1.56(\text{Re.Pr})^{0.333} (D/L)^{0.333}$
- 3C Explain the phenomena of dropwise and film condensation. 02
- 4A Derive an expression for calculating the effectiveness of a counter flow heat 05

exchanger in terms of overall heat transfer coefficient, area of heat exchanger and the heat capacity

- 4B A heat exchanger is to heat water from  $20^{\circ}\text{C}$  to  $60^{\circ}\text{C}$  while water is flowing through tubes of 25mm outer diameter and 20mm inner diameter and 4m long. Heat is supplied by steam condensing outside the tubes at  $100^{\circ}\text{C}$ . The total water flow rate through all the tubes is 680 kg/min and the thermal conductivity of the tube is  $325 \text{ W/m}^{\circ}\text{C}$ . The inside and outside film coefficient can be taken as being  $4100 \text{ W/m}^2\text{ }^{\circ}\text{C}$  and  $800 \text{ W/m}^2\text{ }^{\circ}\text{C}$ . Estimate the total number of tubes required. 05
- 5A Derive expression for intensity of radiation (I) in terms of emissive power of a body (E) 05
- 5B A cryogenic fluid flows through a long tube of 20 mm diameter, the outer surface of which is diffuse and gray ( $\epsilon_1=0.02$ ) at 77K. This tube is concentric with a larger tube of 50 mm diameter, the inner surface of which is diffuse and gray ( $\epsilon_2=0.05$ ) and at 300K. The space between the surfaces is evacuated. Calculate the heat gain by cryogenic fluid per unit length of tube. If a thin radiation shield of 35 mm diameter ( $\epsilon_3=0.02$ ) both sides is inserted midway between the inner and outer surfaces, calculate the percentage change in heat gain per unit length of the tube. 05