Reg. No.

## IANIPAL TUTE OF TECHNOLOGY uent Institute of Manipal University, Manipa

**VII SEMESTER B.TECH (MECHANICAL/IP ENGG.) END SEMESTER** 

# **EXAMINATIONS, NOV/DEC 2017**

SUBJECT: DESIGN OF THERMAL POWER PLANT SYSTEMS (P-6) [MME 4010]

### **REVISED CREDIT SYSTEM**

Time: 3 Hours

#### MAX. MARKS: 50

#### Instructions to Candidates:

- Answer ALL the questions.
- Missing data may be suitably assumed.
- Use of heat exchanger data sheet, thermodynamics and heat transfer data book are permitted
  - **1A.** With a neat sketch explain the furnace based natural loop steam generating 05 unit taking into account various heat exchangers.
  - **1B.** Engine oil flowing at a rate of 2 kg/s need to be cooled from 100°C to 60°C in a double pipe heat exchanger with raw water(entry temperature =  $20^{\circ}$ C, flow rate = 2.04 kg/s) as coolant. The following design data are selected:

Annulus nominal diameter	Π	5", Schedule 40
Inner pipe nominal diameter	Π	<sup>3</sup> ⁄ <sub>4</sub> ″, Schedule 40
Fin height	Π	0.0127 m
Fin thickness	Π	0.90 mm
Number of fins/tube	Π	30
Number of tubes in the annulus	=	2

Calculate oil and water side convective heat transfer coefficient.

- 2A. Explain with neat sketches the different zones of condensation in horizontal tube.
- 2B. A shell and tube heat exchanger is meant for heating treated water by the use of engine oil which enters the tubes at 70°C and 50000 kg/h. As a coolant water enters at 30°C, 30000 kg/h and leaves at 50°C. Two tube pass with total number of 124 tubes is preferred. Tube thickness is 20 BWG. Take baffle spacing as 0.6D<sub>s</sub>. Consider tube side convective coefficient as 15.2 W/m<sup>2</sup>K. Tube material is carbon steel (0.5% C). Don't consider the effect of variable physical property in convective coefficient calculation.

Find the length of the heat exchanger based on TEMA standards.

- 3A. Sketch and explain a natural draught cooling tower. Define various cooling tower parameters.
- **3B.** Air enters at 1 atmosphere and 30°C the core of a circular finned tube matrix (surface CF-872 (C)). The air flows at the rate of 1618 kg/h perpendicular to the tubes and exits with a temperature 90°C. The core is 0.5 m long with 0.25 m<sup>2</sup> frontal area. Calculate the total pressure drop between air inlet and outlet and average heat transfer coefficient on the air side.

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- **4B.** A condenser is to be designed to condense 163 kg/h of steam at atmospheric pressure. A square array of 100, 10 mm outside diameter tubes are available for the design and the wall temperature of the tube is maintained at 98°C.
  - (a) Estimate the length of the tube required (by referring Kern relation), if the condenser is to be installed in the horizontal position.
  - (b) If the above condenser is by mistake installed in the vertical position, will there be any change in the condensation rate? If so find the modified value.
- **5A.** Fired heater is used to heat the process fluid having flow rate of 200000 kg/h from 200°C to 350°C. Assume the stack gas temperature to be 100°C more than the process fluid inlet temperature. Propane (M= 44.1) is used as the fuel with 15 % excess air. Take radiation loss as 4 % and other losses (excluding dry gas loss) as 10 %. Specific heat of process fluid is 2500 J/kgK. Specific heat of CO<sub>2</sub>, H<sub>2</sub>O, O<sub>2</sub> and N<sub>2</sub> are 1.055, 2.014, 0.997 and 1.057 kJ/kg K respectively. Consider 55 % load in radiant section. Allowable maximum radiation heat flux is 30 kW/m<sup>2</sup>. Tube diameter = 210 mm. pitch = 250 mm, H/D = 1.5. Find:

(a) Furnace efficiency

- (b) Radiant zone load
- (c) Height and diameter of the furnace, (d) Number of tubes in radiant zone
- In a cooling tower performance test, the following readings are noted in case 5B. of Forced mode

II	45°C
=	40°C
=	25°C
=	30°C
=	33°C
=	37°C
=	10 lpm
=	300 s

Find:

- (a) Cooling tower duty
- (b) Cooling tower efficiency
- (c) Mass flow rate of air
- (d) Rate of make-up water

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