

MANIPAL INSTITUTE OF TECHNOLOGY MANIPAL (A constituent unit of MAHE, Manipal)

## IV SEMESTER B.TECH. (CHEMICAL ENGINEERING) END SEMESTER EXAMINATIONS, APRIL/MAY 2019

## SUBJECT: HEAT TRANSFER OPERATIONS

## [CHE 2202] REVISED CREDIT SYSTEM

Date : 02/05/2019

Time: 2 – 5 PM

MAX. MARKS: 50

## **Instructions to Candidates:**

Answer **ALL** the questions.

Missing data if any, may be suitably assumed.

| 1A.          | A rectangular fin of length 5 cm, thickness of 1.25 mm extends from a plane wall                     |            |
|--------------|--|------------|
|              | having thermal conductivity as 45 W/m °C, heat transfer coefficient as 56 W/m <sup>2</sup> °C.       |            |
|              | Assuming wall temperature and ambient temperature are at 150 °C and 28 °C                            |            |
|              | respectively find heat transfer rate per unit width of fin.  | (3 marks)  |
| 1 <b>B</b> . | The inside and outside surfaces of a hollow sphere $a \le r \le b$ at $r = a$ and $r = b$ are        |            |
|              | maintained at temperatures $T_1$ and $T_2$ respectively. The thermal conductivity varies             |            |
|              | with temperature as $k(T) = k (1 + \alpha T + \beta T^2)$ . Derive an expression for total heat flow | (A montra) |
|              | through the sphere.  | (4 marks)  |
| 1C.          | Water is passed through an annular space of 5 cm outer tube diameter and 3 cm of                     |            |
|              | inner tube diameter at 0.5 m/sec velocity. Wall temperature of inner tube is                         |            |
|              | maintained at 80°C. Inlet water temperature is 20°C. Find heat transfer coefficient                  |            |
|              | between water and tube.  |            |
|              | Data : Density of water $= 988 \text{ kg/m}^3$   |            |
|              | Specific heat at constant pressure $= 0.993$ k-cal/kg °C.  | (3 marks)  |
|              | Thermal conductivity of water $= 0.557$ k-cal/hr m °C.   |            |
|              | Kinematic viscosity = $0.55 \times 10^{-6} \text{ m}^2/\text{sec}$                                   |            |

| 2A.        | Stainless steel ball of diameter 3 cm is uniformly heated to a temperature of 800°C.                              |           |
|------------|---|-----------|
|            | It is to be hardened by first cooling in an oil bath to a temperature of 100°C and The                            |           |
|            | heat transfer coefficient and the oil bath temperature are 700 W/m <sup>2</sup> °C and 40°C                       |           |
|            |   |           |
|            | respectively. What is the time required for this process? If 100 balls are to be                                  |           |
|            | quenched per minute, determine the heat removal rate from the oil bath per minute                                 |           |
|            | so that its temperature remains constant at 40°C. Properties of Stainless steel are: $k = \frac{1}{2}$            | (5 marks) |
|            | 61 W/m°C, $\rho$ = 7865 kg/m <sup>3</sup> , $C_p$ = 0.46 kJ/kg °C.  | (*)       |
| 2B.        | A 10 mm cable is to be laid in atmosphere of 20°C with outside heat transfer                                      |           |
|            | coefficient 8.5 W/m <sup>2o</sup> C.The surface temperature of cable is likely to be 65 °C due to                 |           |
|            | heat generation within. Will the rubber insulation ( $k = 0.155$ W/ m°C) be effective. If                         | (3 marks) |
|            | yes how much?   |           |
| 2C.        | Explain enthalpy balance in a single effect evaporator  |           |
|            |   | (2 marks) |
| <b>3A.</b> | A large plate of 6 m high and 1.2 m wide is maintained at a constant temperature of                               |           |
|            | 57°C and exposed to atmospheric air at 4°C. Calculate the heat loss by free                                       |           |
|            | convection by the plate.  |           |
|            | Properties of air at an average temperature of 30.5 °C: Density = $1.16 \text{ kg/m}^3$ ;                         |           |
|            | $C_p$ =1.007 KJ/kg °C ; Kinematic viscosity = 15.89 x 10^{-6} m^2/sec; K = 26.3 x 10^{-2} W/m °C                  | (3 marks) |
| <b>3B.</b> | Euglein Cellhurg Angle eu   | (3 marks) |
|            | Explain Colburn Analogy.  |           |
| <b>3C.</b> | A thin aluminium sheet with an emissivity of 0.1 on both sides is placed between                                  |           |
|            | two very large parallel plates that are maintained at uniform temperatures $T_1 = 800 \text{ K}$                  |           |
|            | and $T_2 = 500$ K and have emissivities $\varepsilon_1 = 0.2$ and $\varepsilon_2 = 0.2$ , respectively. Determine |           |
|            | the net rate of radiation heat transfer between the two plates per unit surface area of                           |           |
|            | the plates and compare the result to that without the shield.   | (4 marks) |
| 4A.        | A single effect evaporator is used to concentrate 9070 kg/hr of 20% caustic soda                                  |           |
|            | solution to 50% solids. The gauge pressure of steam is 1.37atm. The absolute                                      |           |
|            | pressure in the vapor space is 100 mm Hg. There is a BPE of 22.78 °C. The overall                                 |           |
|            | heat transfer coefficient is estimated to be 1400 W/m2 °C and the feed temperature is                             |           |
|            | 37.8 °C. Calculate (a) Amount of steam consumed (b) Economy (c) Heating surface                                   |           |
|            | required. Data: Enthalpy of feed at 37.8 °C = $127.9245$ kJ/kg Enthalpy of thick                                  |           |
|            | liquor = 514.0239 kJ/kg Enthalpy of vapour = $2672.46$ kJ/kg Heat of vaporization of                              |           |
|            | $M_{\rm a}$ = 51 1.0257 ks/kg Eminarpy of vapour = 2072.40 ks/kg from of vaporization of                          |           |

| Oslo crystallizer with a neat sketch.Image: A state of the state of th |              | steam at 1.37 atm = 2184.0201 KJ/ Kg Condensation temperature of steam = 126.11°C  | (5 marks) |
|--|--------------|--|-----------|
| exchanger at 0.25 kg/s at 15°C and is heated to 45°C by hot water that enters at 100°C and 3 kg/s. If the overall heat transfer coefficient is 950 W/m <sup>2</sup> °C, determine the heat transfer rate and the area of the heat exchanger by $\varepsilon - NTU$ method. Assume specific heat of water to be 4180 J/kg°C.<br><b>5B.</b> Write short notes on the following:<br>(i) Pool boiling<br>(ii) Nucleation<br>(iii) Dropwise condensation<br>(iv) Kirchoff's law of radiation<br>(v) Mier's Supersaturation theory   | 4 <b>B</b> . |  | (5 marks) |
| <ul> <li>(i) Pool boiling</li> <li>(ii) Nucleation</li> <li>(iii) Dropwise condensation</li> <li>(iv) Kirchoff's law of radiation</li> <li>(v) Mier's Supersaturation theory</li> </ul>  | 5A.          | exchanger at 0.25 kg/s at 15°C and is heated to 45°C by hot water that enters at 100°C and 3 kg/s. If the overall heat transfer coefficient is 950 W/m <sup>2</sup> °C, determine the heat transfer rate and the area of the heat exchanger by $\varepsilon - NTU$ method. | (4 marks) |
| ( <b>6 marks</b> ) ( <b>6 marks</b> )  | 5B.          | <ul> <li>(i) Pool boiling</li> <li>(ii) Nucleation</li> <li>(iii) Dropwise condensation</li> <li>(iv) Kirchoff's law of radiation</li> <li>(v) Mier's Supersaturation theory</li> </ul>  | (6 marks) |