

Reg. No.

--	--	--	--	--	--	--	--	--	--



MANIPAL INSTITUTE OF TECHNOLOGY

MANIPAL

(A constituent unit of MAHE, Manipal)

V SEMESTER B.TECH. ONLINE PROCTORED END SEMESTER

EXAMINATIONS DEC 2021

SUBJECT: MASS TRANSFER II [CHE 3152]

REVISED CREDIT SYSTEM

(23/12/2021)

Time: 75 minutes

MAX. MARKS: 20

Instructions to Candidates:

- ❖ Answer **ALL** the questions.
- ❖ Missing data may be suitable assumed.

1A. A solution of carbon tetrachloride and carbon disulfide containing 50 wt% each is to be continuously fractionated at standard atmospheric pressure at the rate of 5500kg/h. The distillate product is to contain 92 wt % carbon disulfide, the residue 0.8 wt %. The feed will be 40 mol% vaporized before it enters the tower. A total condenser will be used, and the reflux will be returned at the bubble point. The equilibrium data (x, y^* = mole fraction CS_2) is as follows:

Molecular weight of carbon disulfide and carbon tetrachloride are 76 g/mol and 154 g/mol respectively.

T (°C)	x	y*
76.7	0	0
74.9	0.0296	0.0823
73.1	0.0615	0.1555
70.3	0.1106	0.2660
68.6	0.1435	0.3325
63.8	0.2585	0.4950
59.3	0.3908	0.6340
55.3	0.5318	0.7470
52.3	0.6630	0.8290
50.4	0.7574	0.8780
48.5	0.8604	0.9320
46.3	1	1

Determine the number of theoretical trays required at a reflux ratio equal to the twice the minimum.

1B. Dilute ethanol-water solutions can be continuously rectified to give at best the mixtures containing 89.4 mole % ethanol at atmospheric pressure, since this is the composition of minimum boiling azeotrope in the binary system. Ethanol can be further purified either by using n-pentane as entrainer or ethylene glycol as solvent. Write short notes on the methods which uses the above-mentioned compounds in the purification of ethanol and comment on the most desirable method.

1C.	Discuss about spiral wound membranes and bundle of hollow fibers with schematic representation. Also, which among these is generally used in RO systems	03																																																																														
2A.	<p>900 kg of crushed oil seeds (22% oil, 78% meal) is extracted in a three-stage cross-current unit using 600 kg of pure hexane in each stage. The equilibrium data are as follows:</p> <table border="1" data-bbox="199 331 1407 828"> <thead> <tr> <th colspan="3">Overflow (100 kg) solution</th> <th colspan="3">Underflow (100 kg) slurry</th> </tr> <tr> <th>W_A (kg)</th> <th>W_B (kg)</th> <th>W_C (kg)</th> <th>W'_A (kg)</th> <th>W'_B (kg)</th> <th>W'_C (kg)</th> </tr> </thead> <tbody> <tr><td>0.3</td><td>99.7</td><td>0</td><td>67.2</td><td>32.8</td><td>0</td></tr> <tr><td>0.45</td><td>90.6</td><td>8.95</td><td>67.1</td><td>29.94</td><td>2.96</td></tr> <tr><td>0.54</td><td>84.54</td><td>14.92</td><td>66.93</td><td>28.11</td><td>4.96</td></tr> <tr><td>0.70</td><td>74.47</td><td>24.83</td><td>66.58</td><td>25.06</td><td>8.36</td></tr> <tr><td>0.77</td><td>69.46</td><td>29.77</td><td>66.26</td><td>23.62</td><td>10.12</td></tr> <tr><td>0.91</td><td>60.44</td><td>38.65</td><td>65.75</td><td>20.9</td><td>13.35</td></tr> <tr><td>0.99</td><td>54.45</td><td>44.56</td><td>65.33</td><td>19.07</td><td>15.6</td></tr> <tr><td>1.19</td><td>44.46</td><td>54.35</td><td>64.39</td><td>16.02</td><td>19.59</td></tr> <tr><td>1.28</td><td>38.50</td><td>60.22</td><td>63.77</td><td>14.13</td><td>22.10</td></tr> <tr><td>1.28</td><td>34.55</td><td>64.17</td><td>63.23</td><td>12.87</td><td>23.90</td></tr> <tr><td>1.48</td><td>24.63</td><td>73.89</td><td>61.54</td><td>9.61</td><td>28.85</td></tr> </tbody> </table> <p>Calculate the fraction of oil extracted in a three-stage cross-current unit using PS method.</p>	Overflow (100 kg) solution			Underflow (100 kg) slurry			W_A (kg)	W_B (kg)	W_C (kg)	W'_A (kg)	W'_B (kg)	W'_C (kg)	0.3	99.7	0	67.2	32.8	0	0.45	90.6	8.95	67.1	29.94	2.96	0.54	84.54	14.92	66.93	28.11	4.96	0.70	74.47	24.83	66.58	25.06	8.36	0.77	69.46	29.77	66.26	23.62	10.12	0.91	60.44	38.65	65.75	20.9	13.35	0.99	54.45	44.56	65.33	19.07	15.6	1.19	44.46	54.35	64.39	16.02	19.59	1.28	38.50	60.22	63.77	14.13	22.10	1.28	34.55	64.17	63.23	12.87	23.90	1.48	24.63	73.89	61.54	9.61	28.85	05
Overflow (100 kg) solution			Underflow (100 kg) slurry																																																																													
W_A (kg)	W_B (kg)	W_C (kg)	W'_A (kg)	W'_B (kg)	W'_C (kg)																																																																											
0.3	99.7	0	67.2	32.8	0																																																																											
0.45	90.6	8.95	67.1	29.94	2.96																																																																											
0.54	84.54	14.92	66.93	28.11	4.96																																																																											
0.70	74.47	24.83	66.58	25.06	8.36																																																																											
0.77	69.46	29.77	66.26	23.62	10.12																																																																											
0.91	60.44	38.65	65.75	20.9	13.35																																																																											
0.99	54.45	44.56	65.33	19.07	15.6																																																																											
1.19	44.46	54.35	64.39	16.02	19.59																																																																											
1.28	38.50	60.22	63.77	14.13	22.10																																																																											
1.28	34.55	64.17	63.23	12.87	23.90																																																																											
1.48	24.63	73.89	61.54	9.61	28.85																																																																											
2B.	Consider question 2A. Calculate the fraction of oil extracted in a single stage contactor for the same volume (1800kg) of the solvent and comment on the result.	03																																																																														
2C.	Write a short note on any one solid-liquid contacting equipment which does not result in the clogging by fines with neat schematic diagram.	02																																																																														
