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### DEPARTMENT OF CHEMICAL ENGINEERING

III Semester B.Tech. Chemical Engineering

End-Semester Examination – January 2022 (Proctored Online Examination)

CHE 2152: Chemical Process Calculations

### PART B

DATE: 27/01/2022

TIME: 75 + 10 MINUTES

MAX. MARKS: 20

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*Note:* Answer ALL questions. Missing data may be suitably assumed.

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**Q.1A)** A solution containing 25% benzene, 35% toluene and rest xylene is in equilibrium with its vapour at 373 K. All percentages are on a weight basis. Determine the following:

- (a) The total pressure
- (b) The composition of the vapour
- (c) The average molecular weight of the liquid and vapour

(Note: The vapour pressures at 373 K are: benzene = 178.7 kPa, toluene = 74.7 kPa and xylene = 28 kPa. Molecular weight of Benzene is 78.04, toluene is 92.06 and xylene is 106.08 g/mol). [3]

**Q.1B)** At 298 K and 101.3 kPa, air-water vapor mixture has 60% relative humidity. It is then cooled to a temperature of 280 K and compressed to a pressure so that 95% of the water vapour is condensed. The vapor pressure of water at 298 K is 3.1 kPa and at 280 K is 0.964 kPa. Calculate the following: [4]

- (a) The final pressure of the air,
- (b) The volume of final air per cubic meter of original air, and
- (c) Amount of water condensed after cooling the air at 280 K.

**Q.1C)** Tannin is extracted from certain wood bark which contains 6% moisture, 11% tannin, 8 % soluble non-tannin materials and the rest insoluble lignin. After tannin is extracted, the solid residue analyses 1% tannin and 0.25% soluble non-tannin on a dry basis. What is the percent extraction of tannin? [3]

**Q.2A)** A hydrocarbon fuel oil is burnt in furnace. The Orsat analysis of the flue gas obtain after combustion contain  $\text{CO}_2 = 11.2\%$ ,  $\text{O}_2 = 5.8\%$ ,  $\text{N}_2 = 83\%$ . All percentages are by mole. Calculate the (a) wt% of carbon and hydrogen in fuel, and (b) % excess air used for the combustion. Assume that the fuel oil doesn't contain nitrogen. [3]

**Q.2B)** A 1:3 nitrogen-hydrogen mixture is fed to a converter resulting in 20% conversion to ammonia. After the complete separation of ammonia, the remaining unconverted gases are recycled to the converter. The initial reaction mixture contains 0.2% argon by volume. If the limit of argon in the reactor is 5% (by volume) of the  $\text{N}_2\text{-H}_2$  mixture in the reactor, estimate the following: [4]

- (a) The fraction of the recycle that is purged,
- (b) The moles of ammonia produced per 100 moles of feed, and
- (c) The overall conversion of ammonia

**Q.2C)** A natural gas has the following composition on mole basis  $\text{CH}_4 = 83\%$ ,  $\text{C}_2\text{H}_6 = 15\%$  and  $\text{N}_2 = 2\%$ . Calculate the heat to be added to raise the temperature from 300 K to 520 K using heat capacity data given below: **[3]**

$$C_p = a + bT + cT^2 \text{ kJ/ (kmol. K)}$$

<b>Component</b>	<b>a</b>	<b>b x 10<sup>3</sup></b>	<b>c x 10<sup>6</sup></b>
$\text{CH}_4$ (g)	19.26	52.12	11.98
$\text{C}_2\text{H}_6$ (g)	5.41	178.09	- 67.38
$\text{N}_2$ (g)	29.6	5.15	13.19