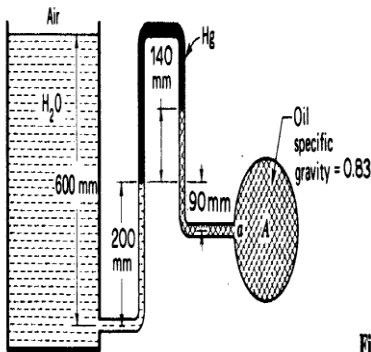
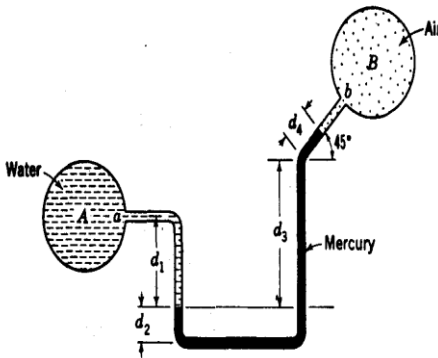
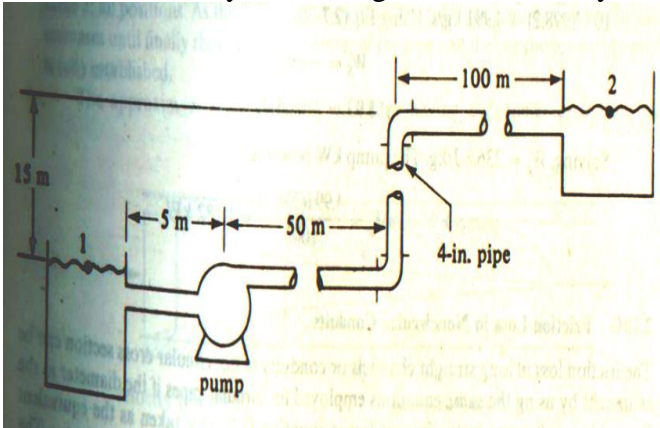




TIME: 3 HOURS

MAX. MARKS: 50

Q. NO	QUESTIONS	M	CO	PO	BTL
1A	<p>For the setup shown in Figure, calculate the absolute pressure at 'a'. Assume standard atmospheric pressure, 101.3 kPa.</p>  <p style="text-align: center;">Fig</p>	4	1	1-3	4
1B	<p>Find the difference in pressure between tanks A and B in Figure, if $d_1 = 330\text{mm}$, $d_2 = 160\text{mm}$, $d_3 = 480\text{mm}$, and $d_4 = 230\text{mm}$.</p> 	4	1	1-3	4
1C	<p>A flat plate of area $1.5 \times 10^6 \text{ mm}^2$ is pulled with the speed of 0.4 m/s relative to another plate located at a distance 0.15 mm apart from it. Find the force and power required to maintain the speed, if the fluid separating them having viscosity of 1 Pa.s.</p>	2	1	1-3	4
2A	<p>A Pitot tube is installed along the axis of a horizontal pipe of 76 mm inner diameter. Air at 40 °C and 105 kPa flows through the pipe. Calculate the rate of flow of air, if the reading of the water differential manometer connected</p>	4	2	1-3	3

	across the tube is 12 mm. Viscosity of air at 40 °C is 0.019 mPa.s. Take $V_{avg}/V_{max}=0.81$ for N_{Remax} between 60000 to 70000.				
2B	A rotameter calibrated for metering has a scale ranging from 0.014 m ³ /min to 0.14 m ³ /min. It is intended to use this meter for metering a gas of density 1.3 kg/m ³ with in a flow range of 0.028 m ³ /min to 0.28 m ³ /min. What should be the density of the new float if the original one has a density of 1900 kg/m ³ ? Both the floats can be assumed to have the same volume and shape.	4	2	1-3	3
2C	Compare the flow measuring devices orifice and venturi meters.	2	2	1-3	2
3A	A centrifugal pump is being tested for performance. and during the test the pressure reading in the 0.305 m diameter suction line just adjacent to the pump casing is 20.7 kPa (vacuum below atmospheric pressure). In the discharge line with a diameter of 0.254 m at a point 2.53 m above the suction line, the pressure is 289.6 kPa gage. The flow of water from the pump is measured as 0.1133 m ³ /s. The density can be assumed as 1000 kg/m ³ . Calculate the kW input of the pump.	5	2	1-3	4
3B	<p>Water at 20 °C is being pumped from a tank at the rate of 5×10^{-3} m³/s. All of the piping is 4" schedule 40 pipe. The pump has an efficiency of 65 %. Calculate only the total friction in straight pipe in J/kg. Given for 4" Schedule 40 pipe, D=0.1023 m. Density = 998.2 kg/m³ and Viscosity=1.005 cP.</p> 	3	3	1-3	4
3C	Water is to flow through 300 m of horizontal pipe at a rate of 0.06 m ³ /s. A head of 6 m is available. What must be the pipe diameter? Take fanning friction factor = 0.0056.	2	3	1-3	5
4A	Consider a device with one inlet and one outlet. If the volume flow rates at the inlet and the outlet are the same, is the flow through this device necessarily steady? Why?	3	3	1-3	4
4B	A fermentation broth with viscosity 10^{-2} Pa.s and density 1000 kg/m ³ is agitated in a 50 m ³ baffled tank using a marine propeller (refer curve 5) 1.3 m in diameter. Calculate the power required for a stirred speed of 4 rps.	3	4	1-3	4
4C	A flat blade turbine agitator with disk having six blades is installed in a tank. The tank diameter is 1.83 m, the turbine diameter is 0.61 m. The tank contains four baffles. The turbine operated at 90 rpm and the liquid in the tank has a viscosity of 10 cP and a density of 929 kg/m ³ . Calculate the required kW of	4	4	1-3	5

	the mixer. Given Data: Width of blade = 0.122 m; and Width of jacket = 0.15 m.				
5A	Calculate the pressure drop of air flowing at 30 °C and 1 atm pressure through a bed of 1.25 cm diameter spheres, at a rate of 60 kg/min. The bed is 125 cm diameter and 250 cm height. The porosity of the bed is 0.38. The viscosity of air is 0.0182 cP and the density are 0.001156 g/cc.	4	4	1-3	5
5B	Particles having a size of 0.1 mm, a shape factor of 0.86, and a density of 1200 kg/m ³ are to be fluidized using air at 25 °C and 202.65 kPa abs pressure. The void fraction at min fluidizing conditions is 0.43. The bed diameter is 0.6 m and the bed contain 350 kg of solids. <ul style="list-style-type: none"> i. Calculate the minimum height of the fluidized bed. ii. Calculate the pressure drop at minimum fluidizing conditions. 	4	4	1-3	4
5C	Calculate the sphericity of a solid particle of a cubical shape.	2	4	1-3	5
	CO: Course Outcome; BLOOM TAXONOMY LEVEL: 1-Remember, 2-Understanding, 3-Application, 4-Analyzis, 5-Evaluation, 6-Creation				