

Exam Date & Time: 03-May-2024 (02:30 PM - 05:30 PM)



MANIPAL ACADEMY OF HIGHER EDUCATION

IV Semester End Semester Examination

MASS TRANSFER -II [CHE 2222]

Marks: 50

Duration: 180 mins.

Descriptive Questions

Answer all the questions.

Section Duration: 180 mins

- 1) Consider Ponchon-Savarit method. Derive the theoretical expressions to determine heat load on condenser, reboiler and the hypothetic stream with a neat schematic diagram (marking all the streams). Also discuss about the significance of the hypothetic stream. (4)
- A)
- B) Dilute ethanol-water solutions can be continuously rectified to give at best the mixtures containing 89.4 mole % ethanol at atmospheric pressure, since this is the composition of minimum boiling azeotrope in the binary system. Ethanol can be further purified either by using n-pentane as entrainer or ethylene glycol as solvent. Write short notes on the methods which uses the above-mentioned compounds in the purification of ethanol and comment on the most desirable method. (3)
- C) What are the assumptions involved in Mc Cabe Thiele (MT) method? Discuss about the graphical and physical considerations in MT method which proves that its assumptions are justified. (3)
- 2) Nicotine (C) in a water (A) solution containing 1% nicotine is to be extracted with kerosene (B) at 20 °C. Water and kerosene are essentially insoluble. Determine the % extraction of nicotine if 100kg of feed solution is extracted using three stages using 50 kg solvent each.
- A)
- | | | | | | | |
|---|----------|---------|---------|---------|---------|---------|
| $x' = \text{kg nicotine/kg water}$ | 0.001011 | 0.00246 | 0.00502 | 0.00751 | 0.00998 | 0.0204 |
| $y'^* = \text{kg nicotine/kg kerosene}$ | 0.000807 | 0.00196 | 0.00456 | 0.00686 | 0.00913 | 0.01870 |
- (4)
- B) Explain heteroazeotropism and its significance in steam distillation with a suitable example. (3)
- C) Derive an expression to theoretically calculate the minimum number of trays if the relative volatility remains reasonably constant throughout the column (provided x_D , x_W and α are known). (3)

- 3) A binary mixture (A and B) are fractionated using a fractionator which has 3 ideal plates. The feed enters between 2nd and the 3rd trays. The feed is a saturated vapor with mole fraction 0.005. The condenser used is a total condenser and the reflux is at its bubble point. The molar rate of reflux is 1.3 moles/mole of feed and rate of vaporization in reboiler is 0.6 moles/mole of feed. The equation for equilibrium line is given as $y = 12.6x$. Calculate the volume and concentration of distillate and the residue. (5)
- A) (3)
- B) Write a short note on any two solid-liquid contacting equipment which does not result in the clogging by fines with neat schematic diagram. (3)
- C) Write a short note on delayed and early feed entry in a distillation column with a schematic representation. (2)

- 4) 1000 kg of crushed oil seeds (19.5% oil, 80.5% meal) is extracted in a three-stage cross-current unit using 500 kg of pure hexane in each stage. Calculate the fraction of oil extracted. The equilibrium data are as follows:

A)

| Overflow (100 kg) solution | | | Underflow (100 kg) slurry | | |
|----------------------------|------------|------------|---------------------------|-------------|-------------|
| W_A (kg) | W_B (kg) | W_C (kg) | W'_A (kg) | W'_B (kg) | W'_C (kg) |
| 0.3 | 99.7 | 0 | 67.2 | 32.8 | 0 |
| 0.45 | 90.6 | 8.95 | 67.1 | 29.94 | 2.96 |
| 0.54 | 84.54 | 14.92 | 66.93 | 28.11 | 4.96 |
| 0.70 | 74.47 | 24.83 | 66.58 | 25.06 | 8.36 |
| 0.77 | 69.46 | 29.77 | 66.26 | 23.62 | 10.12 |
| 0.91 | 60.44 | 38.65 | 65.75 | 20.9 | 13.35 |
| 0.99 | 54.45 | 44.56 | 65.33 | 19.07 | 15.6 |
| 1.19 | 44.46 | 54.35 | 64.39 | 16.02 | 19.59 |
| 1.28 | 38.50 | 60.22 | 63.77 | 14.13 | 22.10 |
| 1.28 | 34.55 | 64.17 | 63.23 | 12.87 | 23.90 |
| 1.48 | 24.63 | 73.89 | 61.54 | 9.61 | 28.85 |

(5)

- B) Write a shot note on the four steps involved in the extraction process with a neat block diagram. (2)
- C) 100 moles of benzene and toluene containing 50 mole% benzene is subjected to a differential distillation at atmospheric pressure till the composition of the benzene in the residue is 33% by mole. Calculate the total moles of the mixture distilled. Assume $\alpha = 2.4$ (3)
- 5) A feed of 1000 kg aqueous solution of pyridine per hour (50% by mass) is to be extracted with pure benzene to reduce the solute content in the raffinate to 2%. Determine the minimum (3)

solvent rate.

A)

| Water layer | | Benzene layer | |
|-------------------|------------------|-------------------|------------------|
| Pyridine (mass %) | Benzene (mass %) | Pyridine (mass %) | Benzene (mass %) |
| 1.17 | 0 | 3.28 | 94.54 |
| 3.55 | 0 | 9.75 | 87.46 |
| 7.39 | 0 | 18.35 | 79.49 |
| 13.46 | 0.15 | 26.99 | 71.31 |
| 22.78 | 0.25 | 31.42 | 66.46 |
| 32.15 | 0.44 | 34.32 | 64.48 |
| 42.47 | 2.38 | 36.85 | 59.35 |
| 48.87 | 3.99 | 39.45 | 56.43 |
| 49.82 | 4.28 | 39.27 | 55.72 |
| 56.05 | 19.56 | 48.39 | 40.05 |

- B) Determine the number of ideal stages required if the solvent rate is 1.3 times the minimum for the data given in question 5 A. (5)
- C) Discuss about the effect of reflux ratio on the condenser and reboiler heat loads with a representation on H-x-y diagram (2)

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